

Title: Balanced Flow Metering and Conditioning Technology for Fluid Systems**Paper Abstract:**

Revolutionary new technology that creates balanced conditions across the face of a multi-hole orifice plate has been developed, patented and exclusively licensed for commercialization. This balanced flow technology simultaneously measures mass flow rate, volumetric flow rate, and fluid density with little or no straight pipe run requirements. Initially, the balanced plate was a drop in replacement for a traditional orifice plate, but testing revealed substantially better performance as compared to the orifice plate such as, 10 times better accuracy, 2 times faster (shorter distance) pressure recovery, 15 times less acoustic noise energy generation, and 2.5 times less permanent pressure loss. During 2004 testing at MSFC, testing revealed several configurations of the balanced flow meter that match the accuracy of Venturi meters while having only slightly more permanent pressure loss. However, the balanced meter only requires a 0.25 inch plate and has no upstream or downstream straight pipe requirements. As a fluid conditioning device, the fluid usually reaches fully developed flow within 1 pipe diameter of the balanced conditioning plate. This paper will describe the basic balanced flow metering technology, provide performance details generated by testing to date and provide implementation details along with calculations required for differing degrees of flow metering accuracy.

Balanced Flow Metering and Conditioning Technology for Fluid Systems (Space Liquid Propulsion Systems)



Anthony R. Kelley

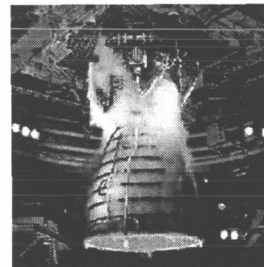
EV23 Advanced Sensors and
Health Management Branch
NASA Marshall Space Flight Center
MSFC, AL 35812
Phone: 256-544-7646
Email: anthony.r.kelley@nasa.gov

11/10/2005

1

Large Rocket Engine Environments

- Very hot (~6000°F)
- Extreme cold (~ -400°F)
- Vibration
- Volatile fluids (liquid oxygen, etc.)
- High pressures (~7,000 psi.)
- Extreme fluid velocities (flow rates, Reynold's numbers $> 10^7$)
- Fast control loops and failure propagation (<3 seconds to full destruction)
- Industry seldom operates in these regimes
- One failed ground test (turbine meter) ~\$200M impact



11/10/2005

2

Problem

- Turbine failure resulted in no LOX flow meter for flight hardware
- Need safe flow metering technology for liquid rocket engines
- Failed past attempts
 - Turbines (work, but severe failure)
 - Vortex shedders
 - Ultrasonic
 - Venturi Tubes (work, but too large for flight)
 - Etc.

11/10/2005

3

NASA Flow Meter Requirements

- Different fluids: LH2, LOX, RP1, etc.
- Different physical states: Gas, Liquid, Multi-Phase
- Wide range (both high and low) in temperature, pressure, vibration and flow conditions
- Very low flow intrusion with near full pressure recovery
- No moving parts
- Minimal piping requirements
- Drop-in replacement of an orifice-plate
- Robust mechanical design
- Highly accurate and repeatable flow measurement
- Easy calibration and maintenance
- Need for high through-put flow areas with low flow restriction

Most needs are common with industrial needs...

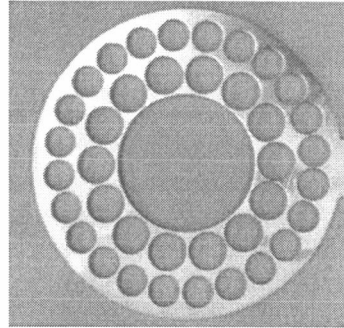
11/10/2005

4

Balanced Flow Meter Solution

- NASA patented technology #10/750,628
- Allows engine measurements where none were before
- Ability to condition or measure flow while improving velocity or other profiles
- Provides flow measurement, conditioning, and controlled restriction performance
- Ability to function with minimal straight pipe run
- Measure mass flow rates, fluid volumetric flow rates and density simultaneously
- Sensor set up can provide a triple redundant measurement system
- Successfully fielded by industry

Possible configuration...



- Beta = 0.9
- 7.5" NDP
- Diff. pressure rated at 150 psi

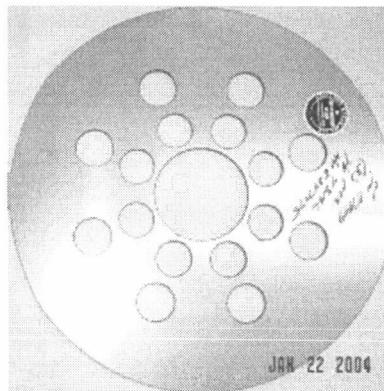
11/10/2005

5

What is Balanced Flow Technology?

- A thin, multi-hole orifice plate with holes sized and placed per a unique set of equations to produce mass flow, volumetric flow, kinetic energy, or momentum BALANCE across the face of the plate

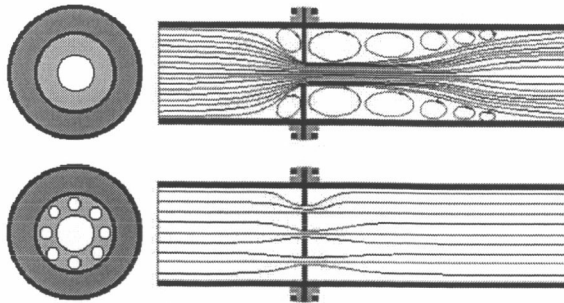
Chevron-Texaco 18
inch Commercial
Plate



11/10/2005

6

How Does It Perform?



Comparison of standard orifice to balanced flow meter, both with 27.1% open area

Results based on compressed gas testing

- 10X better accuracy
- 2X faster pressure recovery (shorter distance)
- 15X noise reduction
- 2.5X less permanent pressure loss
- Exclusively licensed through NASA by A+FlowTek for commercialization

11/10/2005

7

Configurations Tested in 2004



Figure 1 Slotted Configuration

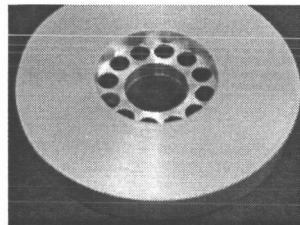


Figure 3 Single Ring of Holes Configuration

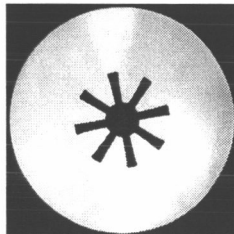


Figure 2 Iron Cross Configuration

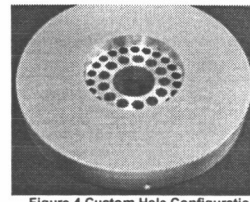


Figure 4 Custom Hole Configuration

Permanent pressure loss, accuracy and discharge coefficient comparable with a Venturi meter!

11/10/2005

8

Balanced Flow Meter Characteristics

- Minimal straight pipe run requirements—BFM has less than 0.5 X pipe diameter straight pipe requirement
- Only requires 0.25 to 0.5 inch thickness and approximately 3 PSI across the plate to condition and monitor flow
- Relatively low cost to build and operate
- Accuracy comparable to Venturi meters

- Cons—similar limitations as standard orifice
 - Not good for pulsing flow
 - Limited turn down
- Testing methods based on American Petroleum Institute (API) Manual of Petroleum Measurement Standards 5.7

11/10/2005

9

How Does it Work?

- **Basic design based on multi-hole orifice plate**
- **Basic relation is the Bernoulli equation**
 - Requires custom Cd calculation
 - Long for Bernoulli equation required for high accuracy applications
 - Highest accuracy applications require physical properties models
- **Flow proportional to SQRT of delta P**
- **Key design factor is the hole distribution**

11/10/2005

10

Technical Basis—BFM Hole Layout

- Plate hole layout basic equation

$$\kappa \rho A V^n = \text{Constant for each hole} =$$

$$(\kappa \rho A V^n)_1 = (\kappa \rho A V^n)_2 = \dots = (\kappa \rho A V^n)_I$$

$$\text{At } \kappa_1 \rho_1 \sim \kappa_i \rho_i$$

$$A_i/A_1 = (V_i/V_1)^n$$

To simplify, let $n = 1$

$$A_i/A_1 = V_i/V_1$$

- Example, given a velocity distribution function

$$V_r/V_{\max} = (1 - R_r/R_{\text{wall}})^{1/7}$$

- Radial velocity ratios

$$V_i/V_1 = ((1 - R_i/R_p)/(1 - R_i/R_p))^{1/7} = A_i/A_1$$

Nomenclature:

- κ : fluid flow correction factor
- ρ : density of fluid
- A : sum of areas at given radius
- V : fluid velocity at radius r
- b : selected balancing constant
- V_{\max} : velocity at $r=0$, pipe center
- R_{wall} : velocity at pipe wall

11/10/2005

11

Technical Basis—BFM Hole Layout Cont.

- Subsequent radial areas

$$A_i = A_1((1 - R_i/R_p)/(1 - R_i/R_p))^{1/7}$$

- Radial area equation

From $\beta^2 = A_{\text{total}} / A_{\text{pipe}}$
And multiple holes,

$$A_0 + A_1 + A_2 + \dots + A_n = A_{\text{total}} = \beta^2 A_{\text{pipe}}$$

- Hole diameters at radius i

$$D_i = (4A_i/\pi N)^{1/2}$$

Shear stresses typically lower than standard, single-hole orifice!

Tech Basis-Bernoulli Equation

- Bernoulli Equation—longer form

$$(P_a - P_b)/\rho + g(Z_a - Z_b)/g_c + (\alpha_a V_a^2 - \alpha_b V_b^2)/2g_c - h_{fb} = 0$$

- Equation of Continuity

$$(\rho AV)_a = m = (\rho AV)_b$$

- Simplified Bernoulli Equation—assume constant density (incompressible), frictionless fluid (zero viscosity), and no elevation changes

$$(P_a - P_b)/\rho + (V_a^2 - V_b^2)/2g_c = 0$$

- Equations from ISO 5167-1, API 14.3.1, etc. Derivations in multiple texts.

11/10/2005

13

Tech Basis-Bernoulli Equation

- Beta area ratio

$$(\beta)^2 = A_b/A_a$$

- Flow Equation

$$m = C_D Y A_b (2g_c \rho_a (P_a - P_b)/(1 - \beta^4))^{1/2}$$

- There can be longer equation forms with many other factors, such as expansion factors, compressibility factors, meter correction factors, etc.

Typical Uncertainties

- Gas Flow: +/- 0.67% (API 14.3.1)
- Liquid Flow: +/- 0.57% (API 14.3.1)
- Spec values are EXTREMELY conservative

BFM Lab Accuracies

- +/- 2% without calibration
- +/- 1.0% long equation
- Calculated +/- 0.1% custom equation, calibrated
- BFM calculated value: +/- 0.25% (Directly measured)

11/10/2005

14

MSFC Water Calibration Facility

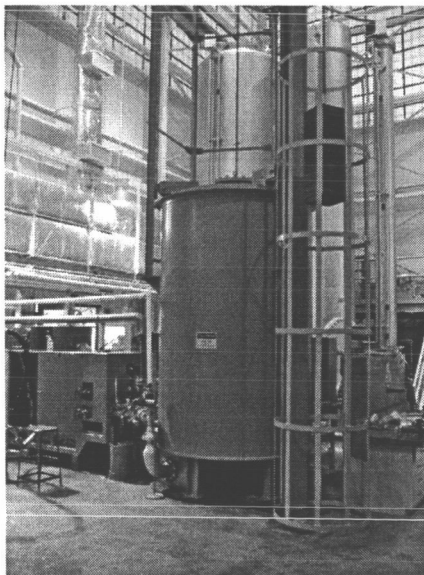


11/10/2005

- National Institute of Standards and Test (NIST) certified
- Volumetric system
- 5000 gallons
- Pump or gravity fed
- Quad deionized water
- 0.25% flow accuracy over unit of time between level sensors
- 0.15% repeatability at given flow set point

15

MSFC Gas Calibration Facility



11/10/2005

- Positive displacement, inverted cylinder system
- NIST certified
- Multiple gases including N, He, Air, Argon, Freon
- 0.01 to 3000 psi operation
- .01 to 400 SCFM
- Accuracy & repeatability???

16

Cd and K Factor Comparisons

Balanced Flow Meter plate performance,
from minimum flows to sonic

| BETA | 0.25 | 0.500 | 0.521 | 0.650 | 0.500,fouled | 0.500,elbow |
|-----------|-------|-------|-------|-------|--------------|-------------|
| Avg Cd | 0.892 | 0.882 | 0.881 | 0.911 | 0.824 | 0.848 |
| Cd Dev | 0.032 | 0.001 | 0.009 | 0.010 | 0.038 | 0.008 |
| Avg K Val | 287.1 | 16.3 | 13.2 | 4.0 | 15.65 | 18.63 |
| K Dev | 20.8 | 0.60 | 0.53 | 0.16 | 1.23 | 0.38 |

| BETA | 0.25 | 0.500 | 0.521 | 0.650 |
|--------------------|-------|-------|-------|-------|
| Venturi K, Cd=0.96 | 134.2 | 5.8 | 4.7 | 1.3 |
| Venturi K, Cd=0.80 | 255.9 | 12.9 | 10.7 | 3.5 |
| BFM K | 287.1 | 16.3 | 13.2 | 4.0 |
| Orifice K | 669.4 | 31.5 | 25.7 | 7.4 |

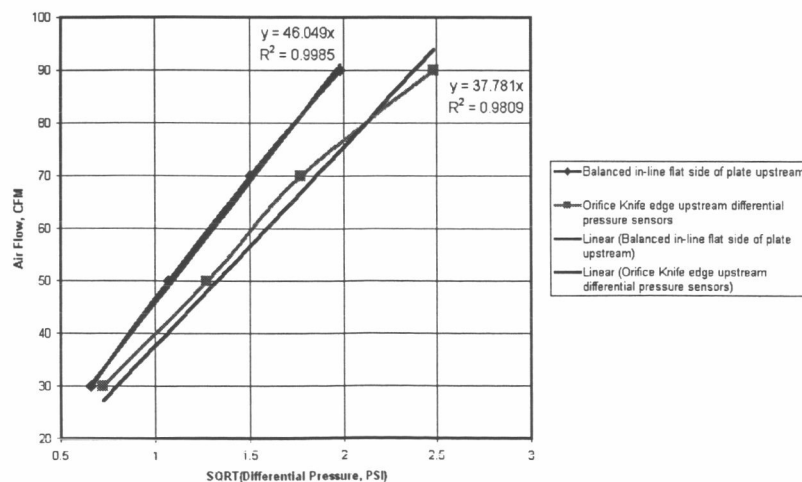
Note: Venturi values do not include downstream losses.

11/10/2005

17

BFM vs. Orifice Flow Equation

SQRT(Differential Pressure, PSI) versus Air Flow, CFM

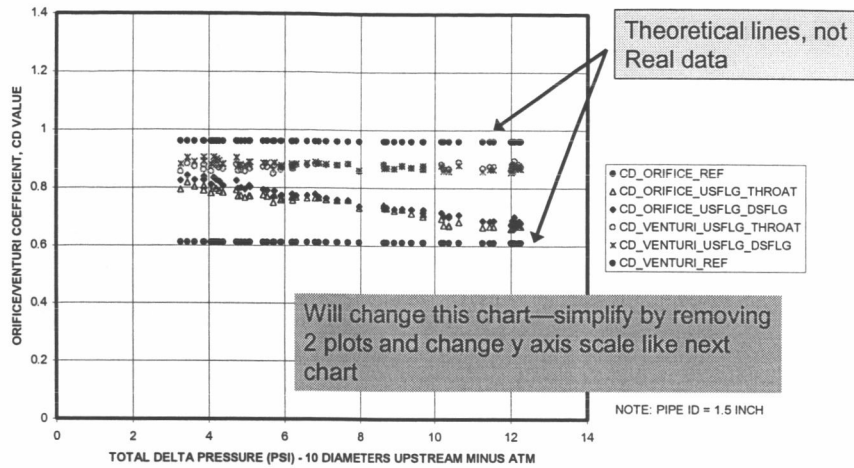


11/10/2005

18

BFM Calibration Cd

ORIFICE/VENTURI COEFFICIENT (Cd) PLOT
Balanced Inline and Staggered beta 0.500 Flat side upstream.xls

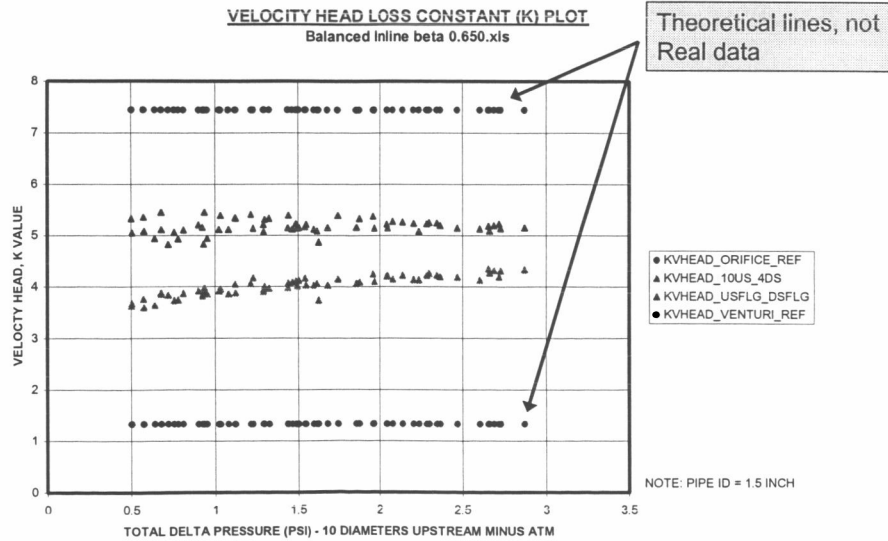


11/10/2005

19

BFM K Factor Plots

VELOCITY HEAD LOSS CONSTANT (K) PLOT
Balanced Inline beta 0.650.xls

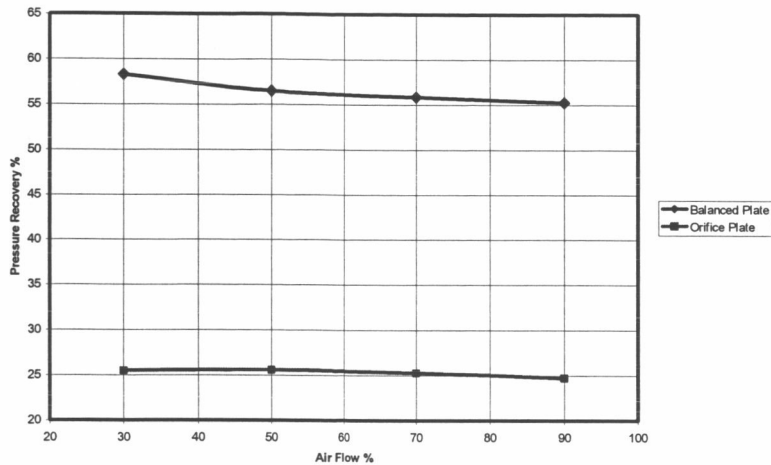


11/10/2005

20

BFM vs. Standard Orifice Pressure Recovery

Pressure Recovery % versus Air Flow %

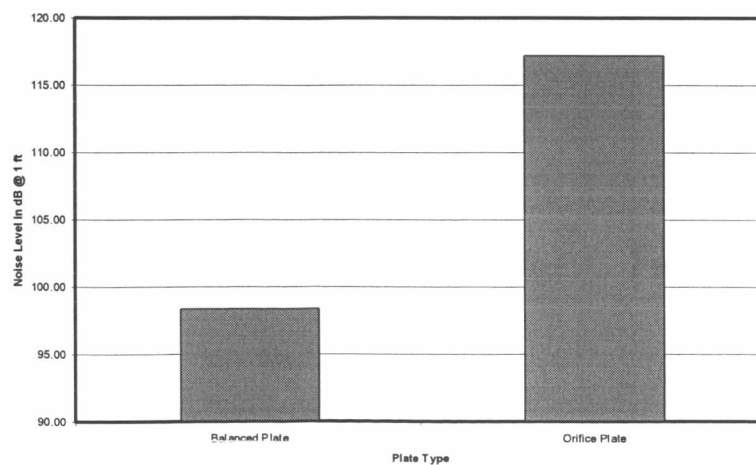


11/10/2005

21

BFM vs. Orifice Acoustic Noise

Flow Meter Noise @ 1 ft and 90% Air Flow



11/10/2005

22

Why Does This Matter?

- Believe will meet NASA liquid engine flow meter requirements—test program on-going
- Provides safe, rugged, robust flow meter
- Provides drop-in orifice meter replacement
- Increases fluid system efficiency to save \$\$\$
- Provides multiple benefits with relative low-cost
 - Reduced piping requirements
 - Reduced noise generation (EPA regulations)
 - No moving parts, simple design
 - Capable of simultaneous fluid metering and flow profile conditioning
 - Robust calibration—well defined and characterized traditional techniques
 - Typical $\pm 0.15\%$ accuracy of measured flow throughout measurement range
 - Reduced pump energy requirements
 - High pressure recovery
 - Low permanent pressure loss

11/10/2005

23

Lessons Learned

- Always double check flow meter vendor claims, flow equations, and calibration techniques
- There are hundreds of emerging flow metering technologies—stringently define your unique requirements
- Determine best calibration method for your application—in-situ system level calibration vs. typical individual component calibration
- Test/Calibrate as you intend to use the meter—If possible, test your new meter!
- Follow standards for instrument placement, uncertainties, etc., but not for plate thickness!

11/10/2005

24

Useful References

- The Consumer Guide to Differential Pressure Flow Transmitters by David W. Spitzer and Walt Boyes, Published by Copperhill and Pointer, Inc., ISBN 1-932095-03-9
- API Manual of Petroleum Measurement Standards 5.7, Testing Protocol for Differential Pressure Flow Measurement Devices
- API Manual of Petroleum Measurement Standards Ch. 14—Natural Gas Fluids Measurement, Section 3—Concentric, Square-Edged Orifice Meters, Part 1—General Equations and uncertainty Guidelines
- API Manual of Petroleum Measurement Standards Ch. 14—Natural Gas Fluids Measurement, Section 3—Concentric, Square-Edged Orifice Meters, Part 2—Specification and Installation Requirements
- ISO 5167-1 Measurement of fluid flow by means of pressure differential devices inserted in circular cross-section conduits running full, Part 1: General principles and requirements
- ISO 5167-1 Measurement of fluid flow by means of pressure differential devices inserted in circular cross-section conduits running full, Part 2: Orifice Plates
- The measurement, instrumentation, and sensors handbook, John G. Webster, CRC Press & IEEE Press

11/10/2005

25

- What about current standards...can we use them or do we have to modify equations?
- Any knowledge of cryogenic calibration facility?

11/10/2005

26